

# Study on Fiber Feeding Mechanism for Direct Extrusion Compression Process

Bommanna K  
 Ph.D Research Scholar,  
 Department of Mechanical Engineering  
 R R Institute of Technology  
 Bangalore, India

Dr K V Mahendra  
 Professor and Principal,  
 Department of Mechanical Engineering  
 R R Institute of Technology  
 Bangalore, India

**Abstract:-** Twin screw extruders have been used for a long time to produce plastic with higher mechanical properties. As of late, the utilization of long fibers has been a development trend, especially for lightweight and durable components.

The rectangular profile extrusions were expelled using a twin-screw expel framework composed of polypropylene and maleated polyolefin. The expulsion procedure was performed to check the properties of these materials.

**Keywords:-** Natural Composite; Twin Screw; Extruder; Chemical Treatment; Coupling Agent.

## I. INTRODUCTION

There are three essential types of extruders in the plastics industry: the hammer extruder, the circle extruder, and the screw extruder. In the plastics industry, a single screw extruder is the most normal type, while a multi-screw extruder is the most notable.

Twin-screw extruders can operate at high or low speed. High speed extruders are typically used for compounding. Low speed extruders are used for profile removal.

Blending occurs in the dissolving zone as long as the strong plastic particles remain in the plug stream. In other words, there is no movement between the plastic particles as they move in the stream.

## II. METHODOLOGY

### A. Extrusion Parameters

Expulsion engineers consider the factors that limit a product's throughput to a quality.

### B. Screw speed

When an item is heat-touchy, keeping up with a high rate can limit home time and boost the item all through. Another reason to restrict screw speed is to prevent air entanglement.

## Continuous Feeding of Fibers

$$\text{Screw speed} = \frac{\text{Targeted weight of fibres}}{\text{length/revolution} \times \text{time} \times \text{weight/length}}$$

Example: Total through put 16 kg/h

Targeted 40% fiber content, 6.4 kg/h  
 fibers

Roving weight: 12 g/m

$$6400 / (0.03 \times 60 \times 12) = 296$$

Screw speed for fiber feeding 296 rpm



### C. Temperature

The temperature constraints in expulsion can be triggered by the presence of sufficient hotness or the failure to utilize enough hotness to get a reliable dissolve.

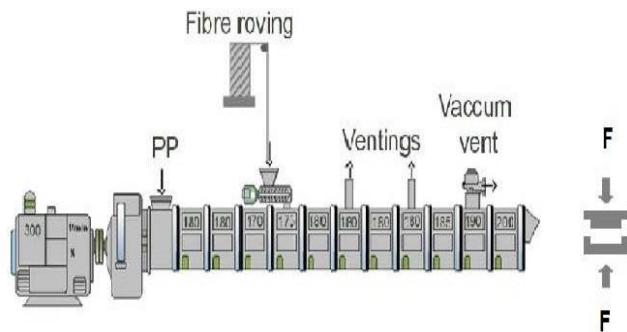


Fig 1: Barrel zones

## III. LITERATURE SURVEY

Panapoy et.al (2000) The effects of screw speed on the temperature profiles of polypropylene melters were studied in a study conducted in 2000 using a simple data logger and a PC. The researchers analyzed the various effects of screw speed on the streams of polypropylene melters.

In 1991, Bradley et.al. focused on the expulsion attributes of various kinds of screws used in the manufacture of polypropylene. The impact of these factors on the maker's desire for limited properties was studied.

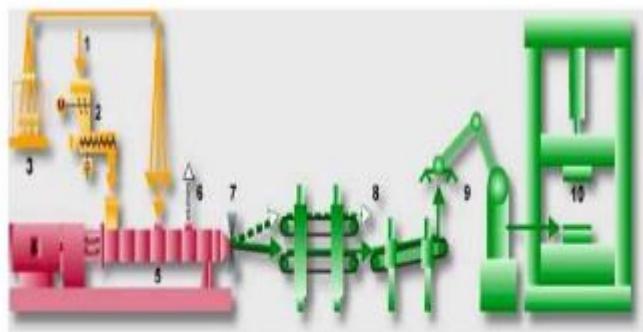
Charlie martin concentrated on twin screw expulsion frameworks for direct long fiber profile expulsion.

Twin screw extruders have been utilized for a long time to intensify a wide range of strands into plastics to improve mechanical properties of the end result. Lately, there has been a development in the utilization of long fiber innovation to produce more grounded and lighter parts, especially for the auto and development markets.

#### IV. TWIN SCREW EXTRUDER DESIGN FOR LONG FIBERPROCESSING

The engine rotates the screws of a twin-screw extruder to provide shear and energy to the object. The gear reduces the engine speed to the appropriate screw rpm while duplicating force, and the circulation gear keeps up with the two screws' rakish planning and ingests the push load from the screw set. Screw speed (rpm), feed rate, temperatures along the barrel and kick the bucket, and vacuum level are all part of the cycle control boundaries. Soften pressure, liquefy temperature, engine amperage, and explicit energy use are all common readouts.

A comparable essential cycle capability is performed by any twin-screw extruder, notably dissolving, blending, venting, and cooling.



- |                                      |                                   |
|--------------------------------------|-----------------------------------|
| 1. Polymer                           | 7-8. Cutting and separation units |
| 2. Gravimetric feeding               | 9. Handling system                |
| 3. Fiber roving                      | 10. Compression moulding          |
| 4-6. Co-rotating twin screw extruder |                                   |

*Fig 2: Feeding of long fibers into the extruder*

The length to measurement proportion, or L/D, is a common expulsion phrase. This is the screw's length divided by the measurement. Sectioned screws are gathered on splined and pounded shafts in twin-screw extruders. To avoid material corruption and maintain the ideal dissolve consistency inside the interaction segment, the specific barrel sections are electrically warmed and cooled by fluid, with cooling exhausts inside the barrel and near the liquefy stream.

In a twin-screw extruder, rough wear is limited in the solids-passing on and mixing segments. Vanadium carbide adjustments of preparations are commonly used for screw components and plying blocks to prevent wear. Many approaches, including the use of nickel-based compounds, are used to combat erosion and wear at the same time, as may be required for manufacturing regular strands. Tungsten carbide trims can be used on barrels to provide the best wear resistance. Dealing with shear strain inside the cycle region might be just as important as choosing the right metallurgies to combat wear.

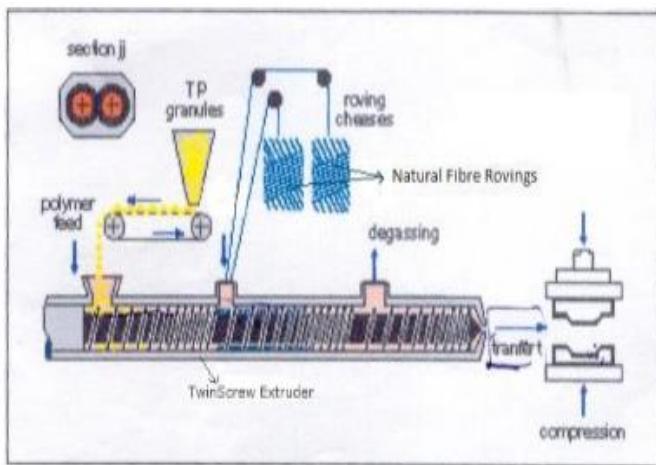
For long fibre compounding, the bi-lobal corotating twin-screw extruder is the industry standard. The screws are self-cleaning, and the material follows a figure eight pattern all the way down the length of the screws. There appears to be an infinite amount of screw plan variations to choose from. However, there are only three basic types of screw components: flighted components, blending components, and drawing components. Material is moved past barrel openings, via blenders, and out of the extruder by flighted screws. Similarly, for wide running definitions, the twin-screw extruder can do dispersive blending right away in the process, with the latter portion of the cycle length being devoted to long fiber blending/devolatilization.

It's possible that blending components will disperse them. Smaller massage components are more distributive, with faster dissolving division rates and less elongational and planar shear. Distributive blending components allow divisions to be liquefied with little extensional shear, which is particularly useful when blending hot and shear-delicate materials.

Keeping fibre lengths constant results in optimal actual qualities in the last part, but it's a challenging task. The filaments will be long if the packages aren't opened very much, but the actual properties will be poor due to the fact that the strands aren't wetted. If filaments are dragged out of groups and heavily wetted, the procedure for separating and wetting them may also result in excessive breaking. To achieve delicate wetting and fibre group opening, the rovings are subjected to mostly distributive blending in order to obtain the proper fibre length.

The choice of screws in the twin-screw extruder controls the tension angle. The feeders control the throughput rate, which is completely independent of the extruder screw rpm. Flighted components are purposefully placed so that the screw channels are not completely filled under the vent/feed sections, which aids downstream filament management and prevents vent flooding.

Devolatilization is also quite successful with twin-screw extruders. For the expulsion of surface moisture that is inherent to glass filaments, a back vent is often sufficient. A downstream vent is possible, and is required for regular filaments due to their proclivity for becoming moist.

*Fig 3: Feeding mechanism*

A gum extruder, in which thermoplastic gum is liquefied, and a compounding extruder, in which liquid thermoplastic pitch is blended in close contact with long supporting strands of roughly one inch long, are part of a mechanical assembly for increasing thermoplastic tar and creating filaments. The extrudate from the compounding extruder is a homogeneous, liquid mass of thermoplastic tar with discrete lengths of filaments arbitrarily scattered in it, and the preforming apparatus includes means for shaping said extrudate from said compounding extruder into a lengthened billet, said preforming apparatus having a release end through which a deliberate volume of an extended billet containing a homogeneous combination of thermoplastic sap and constructing filamen can be released. Furthermore, a remove blade situated for development across said release end of said preforming gadget to slice said prolonged billers to predetermined lengths appropriate for gathering in a pressure forming machine and a pressure shaping machine situated adjacent to said preforming gadget and transport plate implies situated promptly contiguous said release end of said preforming gadget and reversibly versatile between said preforming gadget and said pressure forming machine.

## V. CHEMICAL TREATMENT ON INTERFACIAL ADHESION

Antacid treatment of cellulosic filaments, also known as mercerization, is the most common method for producing high-quality strands. Because of the removal of normal and counterfeit pollutions, soluble base treatment improves the fiber-framework attachment. Furthermore, soluble base treatment promotes fibrillation, which causes the composite fibre pack to separate into smaller strands. Finally, antacid treatment reduces fibre breadth and, as a result, increases the angle proportion. In this way, a better fiber-grid interface bond and an increase in mechanical characteristics are possible thanks to the improvement of an uncomfortable surface geography and an increase in perspective proportion. Soluble base treatment improves mechanical interlocking and the amount of cellulose exposed on the fibre surface by increasing surface discomfort. This increases the number of possible response locations and improves fibre wetting.

*Fig 4: Preparation of NaOH solution*

Normal filaments treated with a soluble base supported the support in the epoxy lattice in the composite appearance, resulting in a magnificent compound bond and improved interface grip, and therefore increased the elasticity of Hybrid composite samples. We can clearly ingest the treated fiber's fibre wetness, as well as a superb fiber-framework and partnership.

*Fig 5: Soaking of fiber in NaOH solution**Fig 6: Cleaning with Distilled water Silane Treatment*

To modify the fibre surface, silane is used as a coupling specialist. During the treatment cycle with the fibre, it goes through several phases of hydrolysis, accumulation, and bond arrangement. Silanols form in the presence of moisture and hydrolysable alkoxy groups. This co-reactivity allows for subatomic advancement over the composite's interface. It also provides the hydrocarbon chain, which prevents fibres from expanding into the grid.



*Fig 7: Drying in room temperature*

Normal filaments have micropores on their surfaces, while silane coupling specialists act as a surface covering that infiltrates into the pores and creates a tightly interlocked surface covering. In comparison to soluble treated fibre composites, silane treated fibre supported composites have better stiffness qualities.

## VI. UPSTREAM SYSTEM CONSIDERATION

Feeders are an essential component of any twin-screw expulsion system. Maintaining plan consistency, maintaining a consistent throughput, delivering precisely aligned fixes, and regulating the cycle's mass exchange attributes are all critical capabilities. Gravimetric controls balance the feed component in order to maintain a steady mass stream to the extruder, based on a computation based on material utilisation as calculated by a heap cell. It can be difficult to control fibre delivery to the twin-screw extruder. While gravimetric control of fibre results from rolls is possible, formula control can accept a specified weight for each length of meandering, which can be validated and adjusted on a regular basis by breaking down the final result.



*Fig 8: Twin screw extruder*

Individual roving weight per length variations will be mitigated by the number of rovings used. VC will fall into some reach, depending on the fibre and the plan of the extruder consumption framework, which for discussion may be:

115% VC > VR > 90% VC

This reach permits genuinely straight forward control of the rate by the change of VR the meandering velocity and the wandering consider required.

Consider the following scenario: the framework is delivering a consistent state while running at a particular wandering count and pace, but a meandering bundle has run out. As a result, the speed, VR, increases, and another wandering is added. When the new substitution is completed, VR maintains its current pace in order to meet the target all-out rate.

## VII. CONCLUSION

If a larger fibre throughput rate is necessary, an increase in meandering count is also a viable option. Rovings are included into the cycle in a semi-natural or physical manner, depending on the interaction. Because of their low cost, high explicit strength, and biodegradability, regular strands can be used to make plastics, but their use has been limited by temperature affectability, dampness debasement, quality variation, helpless surface attachment to hydrophobic polymers, and partition from polymer during expulsion forming. These flaws contribute to the composite's lacklustre presentation. Several studies have looked into the effects of retting, real modifications, and drug pre-treatments on composite properties to address the first four issues, but few have looked into the process of expulsion intensification, which affects the last two. As a result, the goal of this evaluation was to focus on expulsion compounding and its bounds (barrel zone temperature and screw speed) as a solution to these problems, ensuring that the regular strands were uniformly spread inside the chamber, resulting in better extrudates and composites.

## REFERENCES

- [1]. Q. Yuan, D. Wu, J. Gotama and S. Bateman (2008), *Journal of Thermoplastic Composite Materials*, 21, 195.
- [2]. F.L. Matthews, R.D. Rawlings (1994), *Composite Materials: Engineering and Science* London: UK: Chapman & Hall .
- [3]. Klaus Gleich, C.A. Lawton (2001), “Extrusion/Compression of Long Fibre Thermoplastic Composites”, SPE Antec 2001.
- [4]. Daniel Schwendemann, Coperion Werner and Pfleiderer, Stuttgart (2002) “New Developments in Co-Rotating Twin-Screw Extrusion for production of Long natural Fibre Composites”, SPE Antec 2002. [http://www.speautomotive.com/SPEA\\_CD/SPEA2002/pdf/b04.pdf](http://www.speautomotive.com/SPEA_CD/SPEA2002/pdf/b04.pdf)
- [5]. Robert C Constable and Louis N. Kattas (2002), “Long natural Fibre Composites: Rapid Growth and Change”Antec 2002, S. Francisco, USA.
- [6]. K.P.Sigl, H.G.Fritz, (1999) “Compounding of Long natural Fibre Reinforced PP (DIF-LFT) on a Single-screw Extruder”, SPE Antec, Vol.2.
- [7]. Marvin J.Voelkar and Charles D.Weber. “CPI-In-Line compounding systems”. SPE ANTEC-2001: Dallas, TX Paper-185.

- [8]. Alexis Bricout. "Processing and benefits of commingled natural fibre reinforced thermoplastic composites". ANTEC.
- [9]. Shean-wei Yang and Wei-kuo Chin. "Mechanical properties of aligned long glass fibre reinforced polypropylene. 1: Tensile Strength". Polymer Composites, April 1999, Vol.20, No.2, 200-206.
- [10]. Gleich. K (2001), "Extrusion/Compression of long fiber thermoplastic composites".Antec 2001,PP.2065-2